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Stepping Stones to FLNG – The Tassie Shoal Project

Australasian FLNG/FPSO Forum

Perth, 21-22 September 2009

Onshore LNG liquefaction

“Size matters” *

- Why? – because projects include:
 - Separate upstream production facilities
 - Pipelines to shore
 - Land access costs
 - Major environmental footprint
 - Site preparation
 - Rock art relocation
 - Australian fabrication costs
 - Remote locations
 - Site restoration costs



- **Economies of scale are essential to make them attractive**

* D. Voelte - UBS Australian Resources and Energy Conference, 19 June 2009, Sydney



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FLNG is a great idea

(that's why we're here)

- Why? – because projects **Exclude**:
 - Separate upstream production facilities
 - Pipelines to shore
 - Land access costs
 - Major environmental footprint
 - Site preparation
 - Rock art relocation
 - Australian fabrication costs
 - Remote locations
 - Site restoration costs

Plus:

- Technically achievable
- Economically attractive
- Mitigate resource risk (because they can be moved)



Image courtesy of SMBLinde

So why aren't any operating yet?

“Intellectuals solve problems.....” - A. Einstein

Since the '80s the industry has been overcoming:

- Movement Issues:
 - Processing equipment
 - Storage sloshing
 - Offloading challenges
 - Large gas swivel
- Proximity of staffing
- Infrastructure expandability
 - Leveraging resource growth
 - Capturing economies of scale
- Costs

- **BUT** – the industry is poised for breakthrough





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FLNG is not the only great idea

“Intellectuals solve problems, geniuses avoid them” - A. Einstein

An alternative niche idea:

- ~~Movement Issues:~~
 - ~~Processing equipment~~ ✓ Avoid
 - ~~Storage sloshing~~ ✓ Avoid
 - ~~Offloading challenges~~ ✓ Solve
 - ~~Large gas swivel~~ ✓ Avoid
- ~~Proximity of staffing~~ ✓ Avoid
- Infrastructure expandability ✓ Allow
 - Leverages resource growth ✓ Allow
 - Captures economies of scale ✓ Allow
- Costs ✓ Reduce



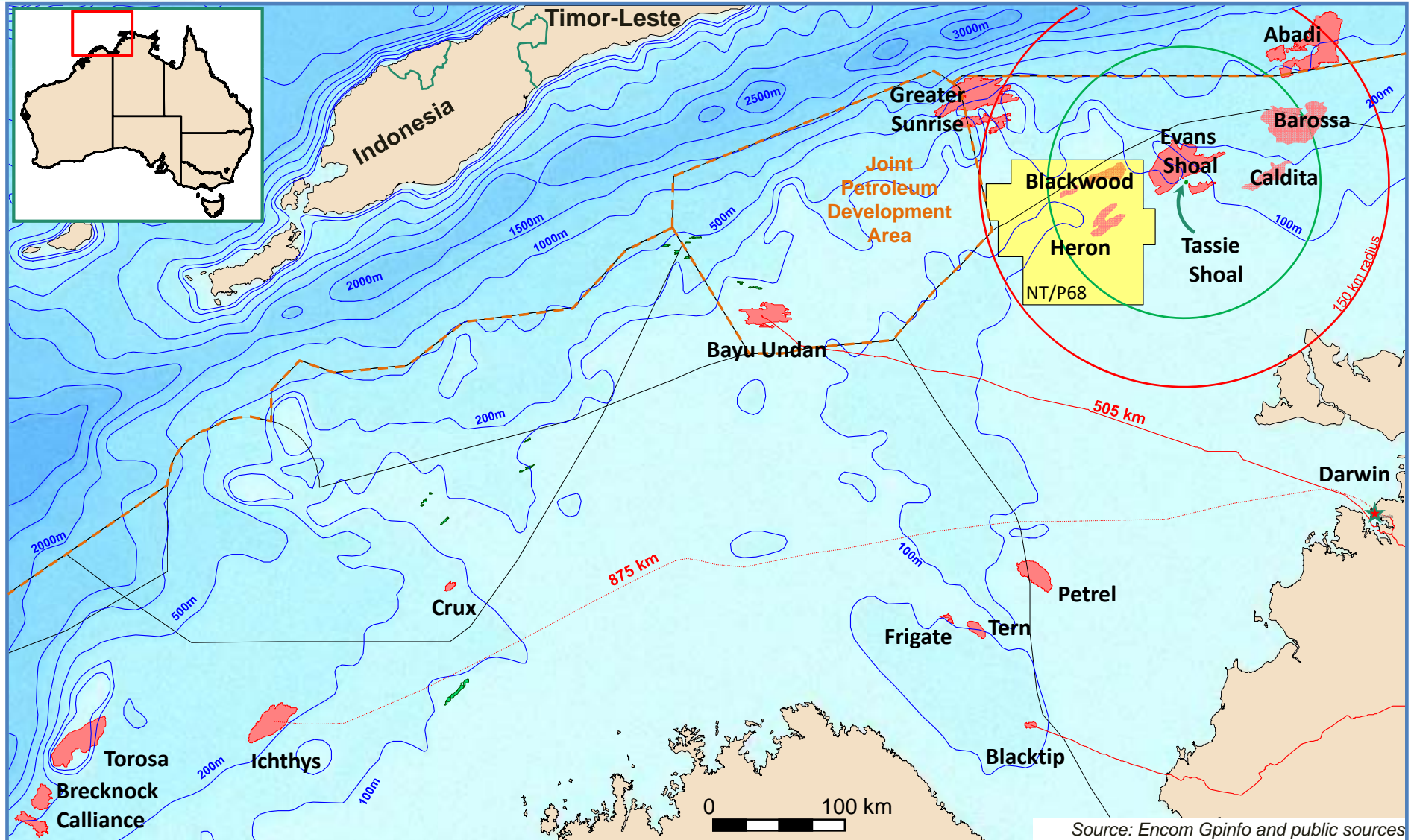
Timor Sea LNG Project
at Tassie Shoal



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Tassie Shoal Location

Centrally located amongst several undeveloped gas fields



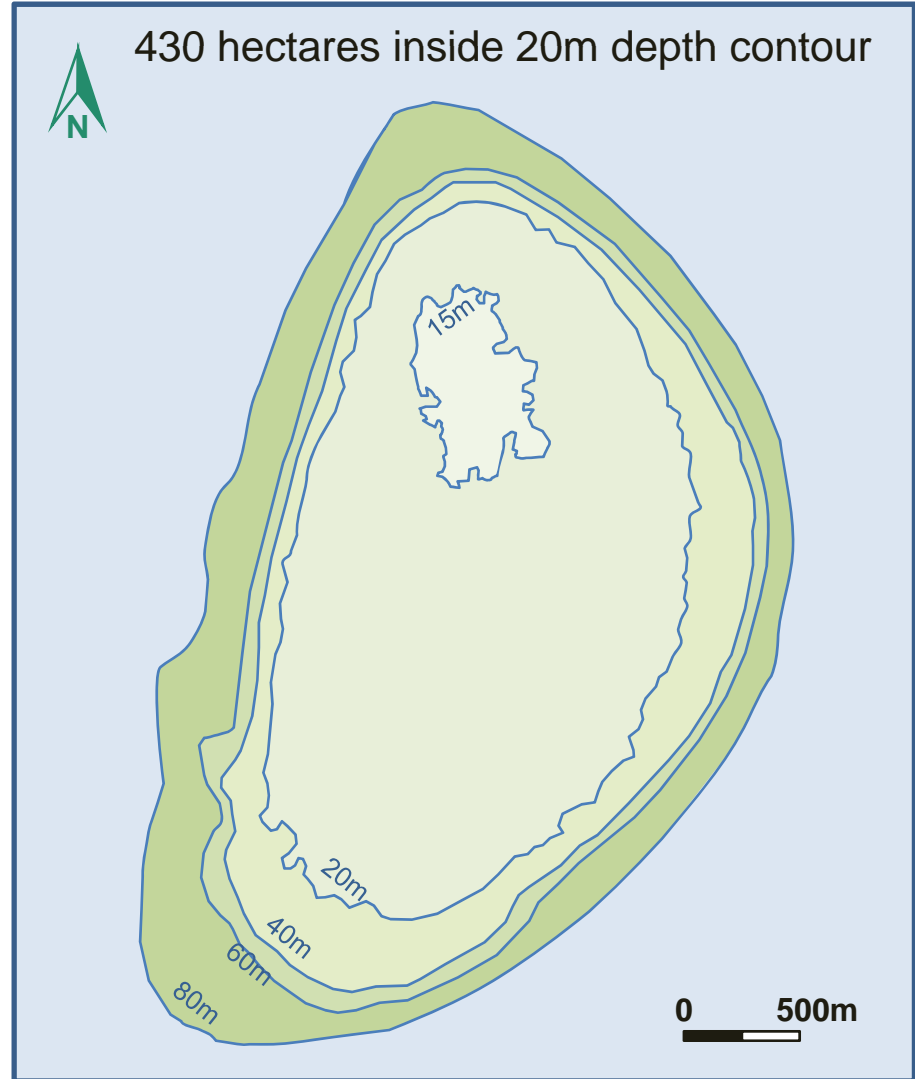
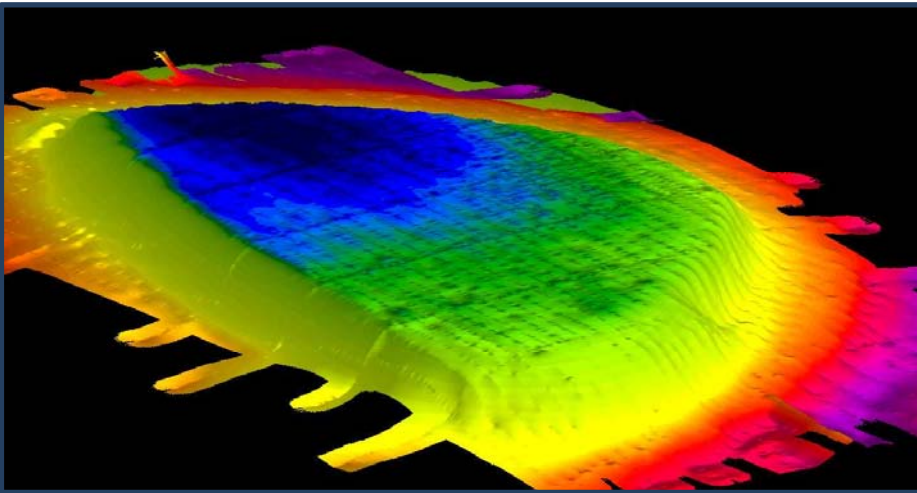
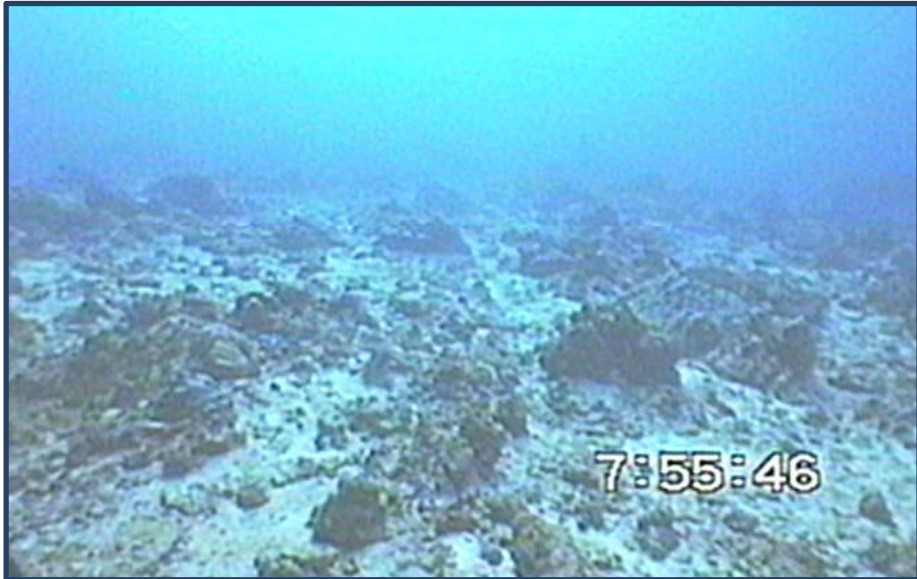


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Tassie Shoal

430 hectares of prime real estate





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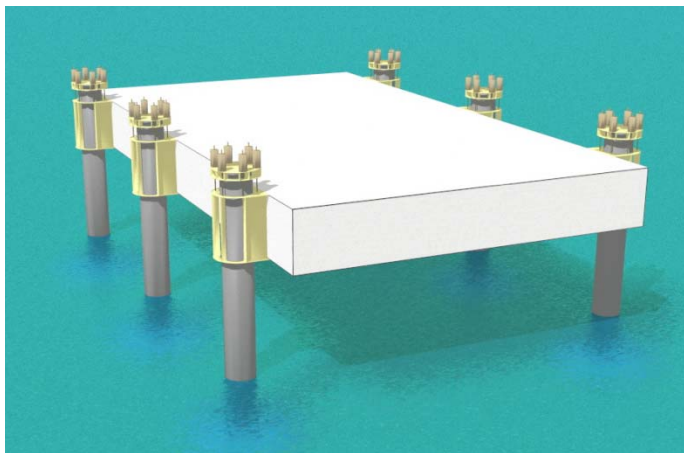
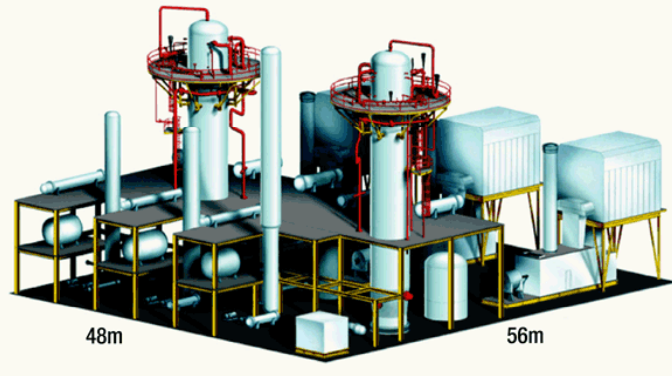
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The LNG Plant

Combination of two established designs

**Air Products' CL DMR FPSO Concept with
MCR® Cryogenic Heat Exchangers**

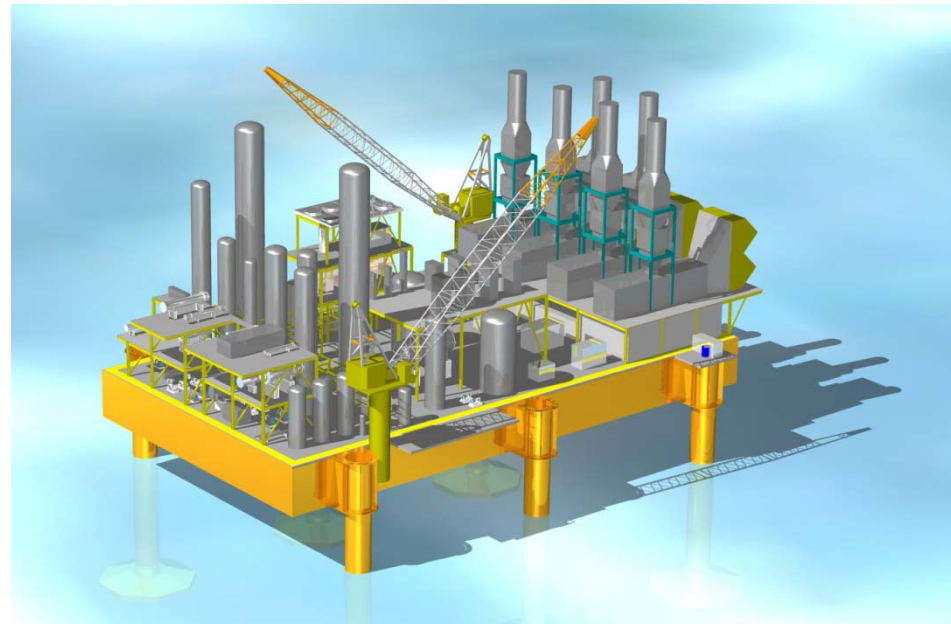
Nominal 3 MTA Capacity



Arup Concept Elevating (ACE) Platform



Air Products/Aker Kvaerner 1990's Concept



Timor Sea LNG Plant

Timor Sea LNG Project

One module



A NWS Train 5 (4.4 Mtpa) module.
Pluto I (4.3 Mtpa) has **264 modules**.



Darwin LNG Plant (3.7 Mtpa)
Timor Sea LNG Plant (3.0 Mtpa) at same scale – **1 module**

- Plant to be fabricated and pre-commissioned at SE Asian location and delivered as **one entire module**
- Indirect seawater cooling using of compact exchangers
 - up to 1/25th plot area of air coolers



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170,000 m³ LNG Storage

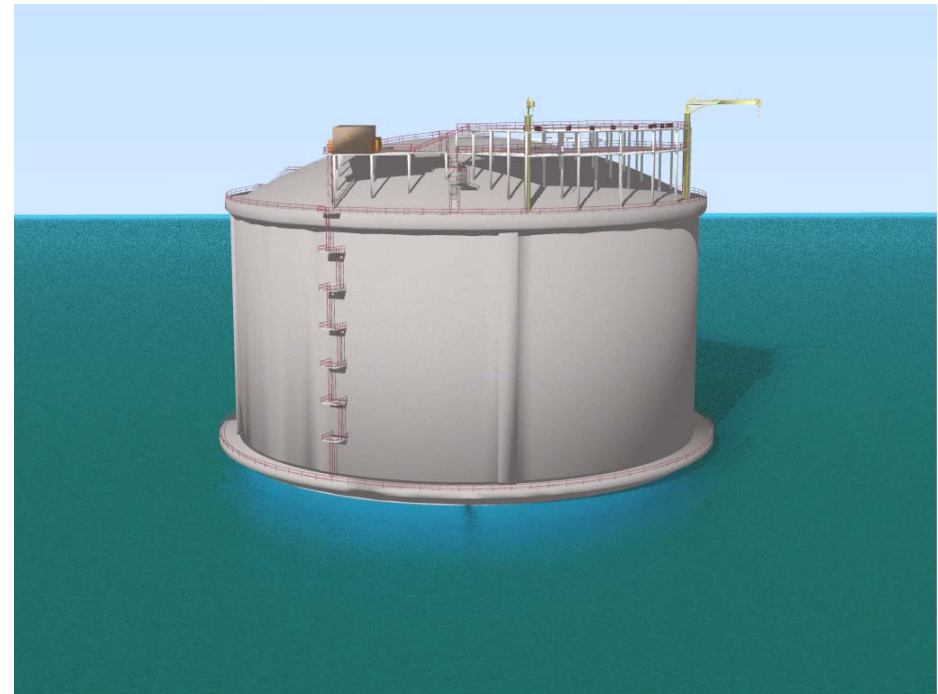
Combination of two proven technologies



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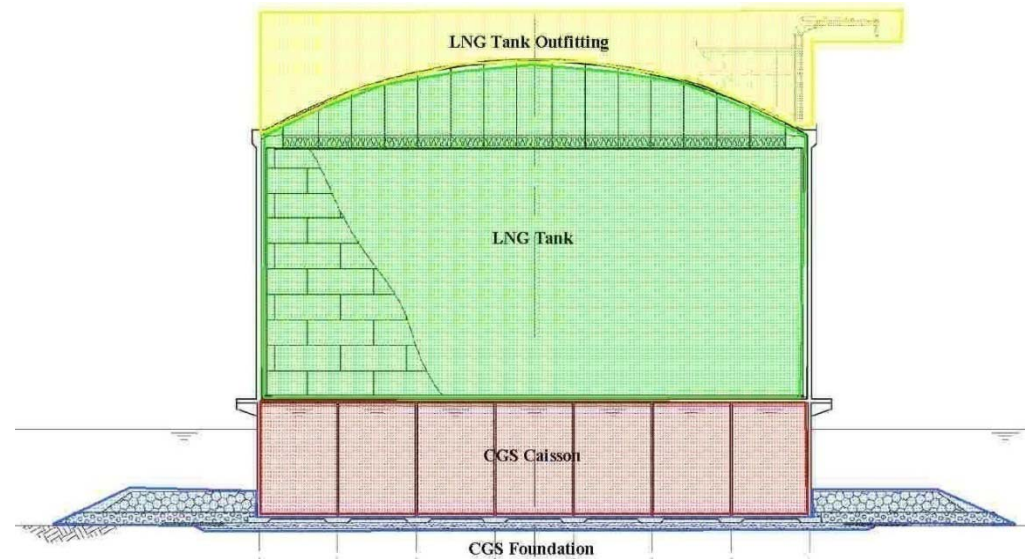
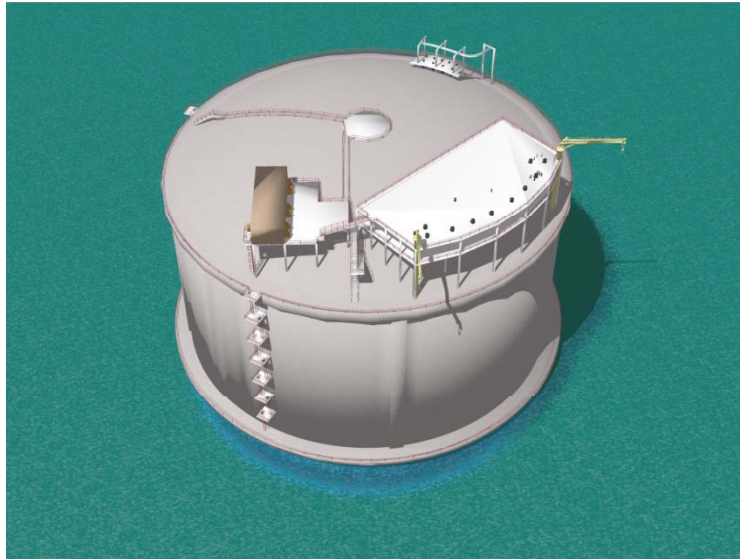




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170,000 m³ LNG Storage

Capacity for additional plant at Tassie Shoal



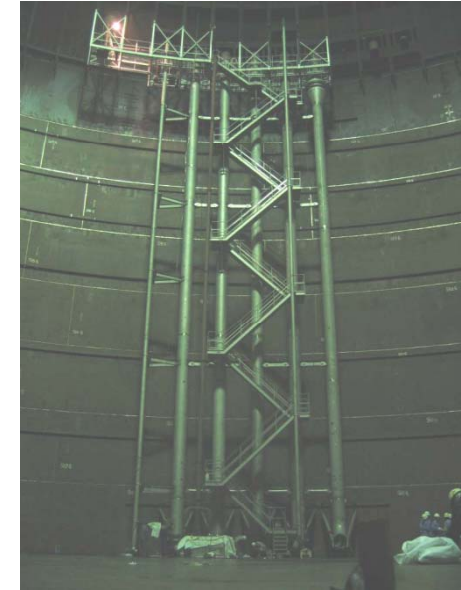
- ArupEnergy Design optimised via secondary follow-up study
- Conventional secondary containment tank on concrete GBS caisson
- Conventional 9% nickel steel LNG tank inside
- Small topside included on tank for LNG handling and export systems
- Water ballast within the CGS caisson for offshore foundation stability



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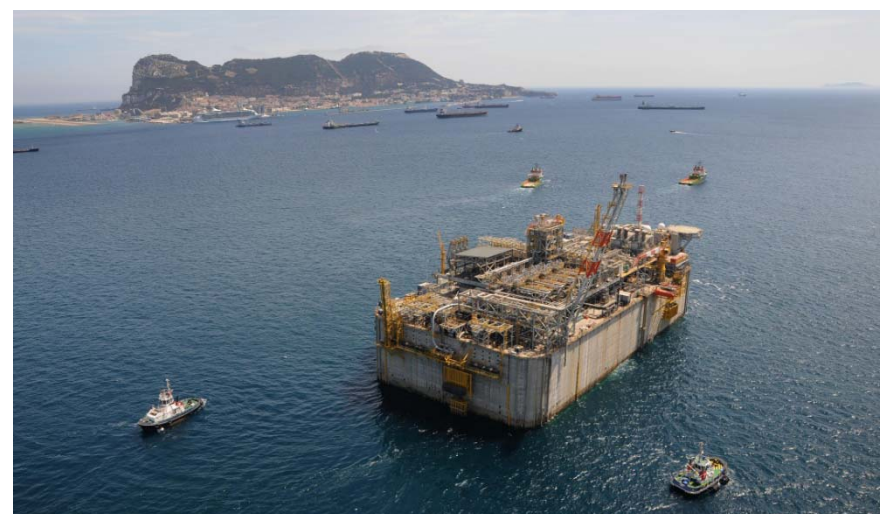
Timor Sea LNG Project

LNG Storage



LNG Storage on a GBS

ExxonMobil Adriatic re-gas terminal





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Accommodation and Control Platform

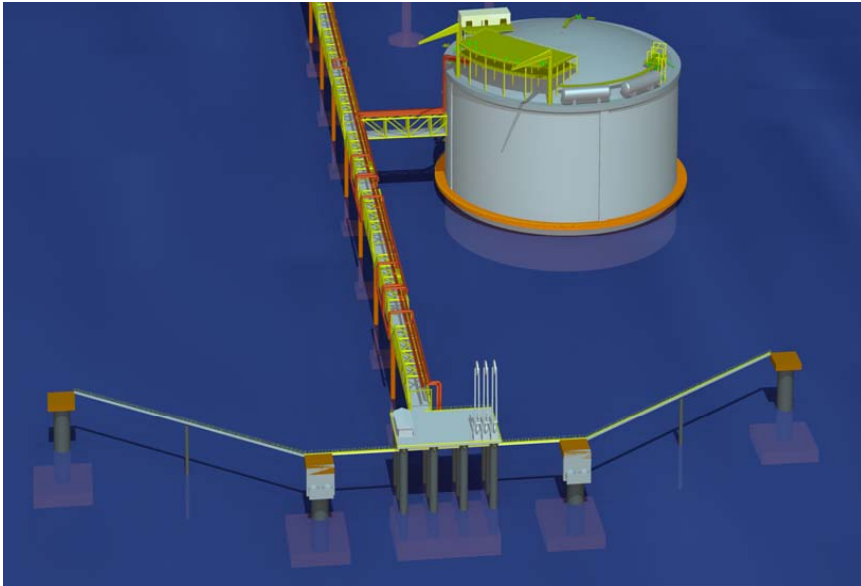
Separate from plant and storage



- Bridge connected to production/processing plant
- Float over or ACE platform selection to be made during FEED

Load-out Options

Conventional or TORP HiLoad



- Initial studies based on conventional loading jetty
- TORP HiLoad is preferred option:
 - Avoids close proximity of vessels to plant and storage
 - Can connect to any standard carrier without modification
 - Avoids requirement for tugs on location
 - Is independent of tides, currents or weather
 - Net cost saving over project life



>US\$1bn capex saving vs onshore plant

Study compared like for like

Estimated costs (US\$M)	Darwin LNG	Tassie Shoal LNG	Potential Savings
Plant Costs	1,549 (WorleyParsons est)	1,090 (WorleyParsons est)	459
Pipeline *	943 (WorleyParsons data)	288 (WorleyParsons data)	655
LNG Tank	300 (MEO est)	330 (Arup est)	(30)
Loadout/Jetty	200 (MEO est)	277 (TORP est)	(77)
Project Development & Owners Costs (6.25%)	188 (same % as TSLNGP)	106 (Fluor/APCI/MEO est)	82
Total Project Cost	\$3,180m	\$2,091m	\$1,089m

- WorleyParsons prepared detailed cost estimates for LNG Plant at Tassie Shoal
- Commissioned to compare costs for functionally similar LNG liquefaction plant at Darwin
- Plant costs savings driven by higher Australian construction costs vs SE Asian construction and commissioning
- Pipeline savings are distance based

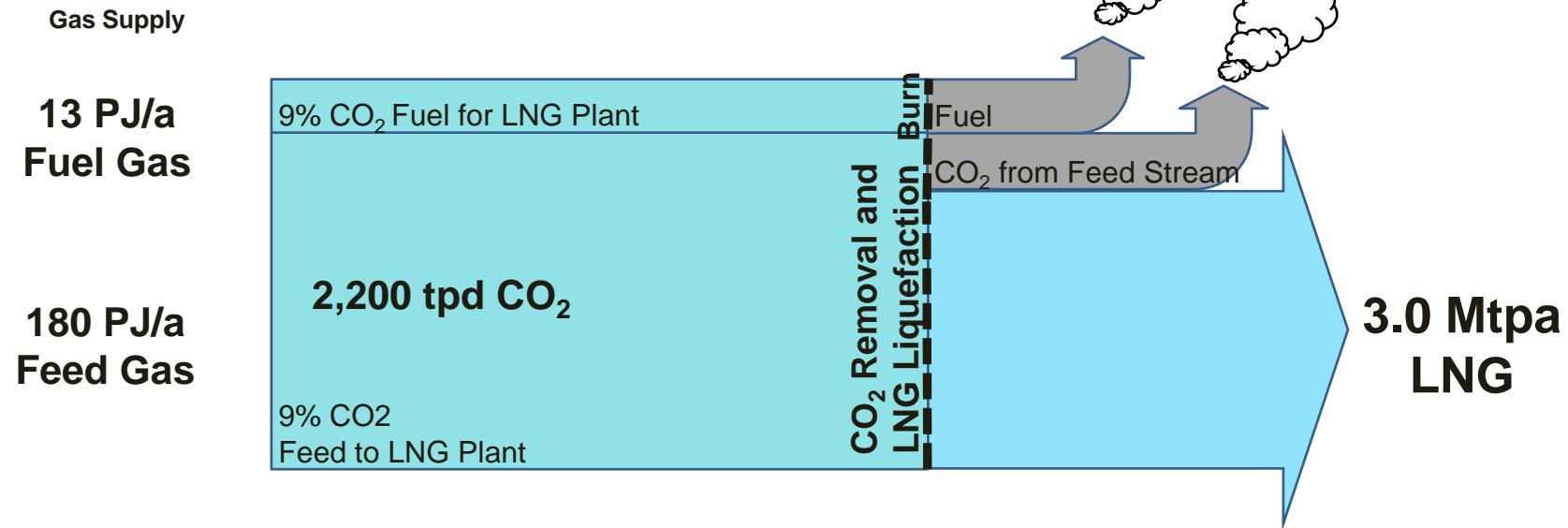
* Based on pipeline from Greater Sunrise to Darwin vs Greater Sunrise to Tassie Shoal

What about CO₂?

“The forgotten challenge” *

tpd CO ₂	Source
170	(carried)
1,830	(combustion)
2,000	(total)

tpd CO ₂	Source
2,200	(carried)
0	(combustion)
2,200	(total)

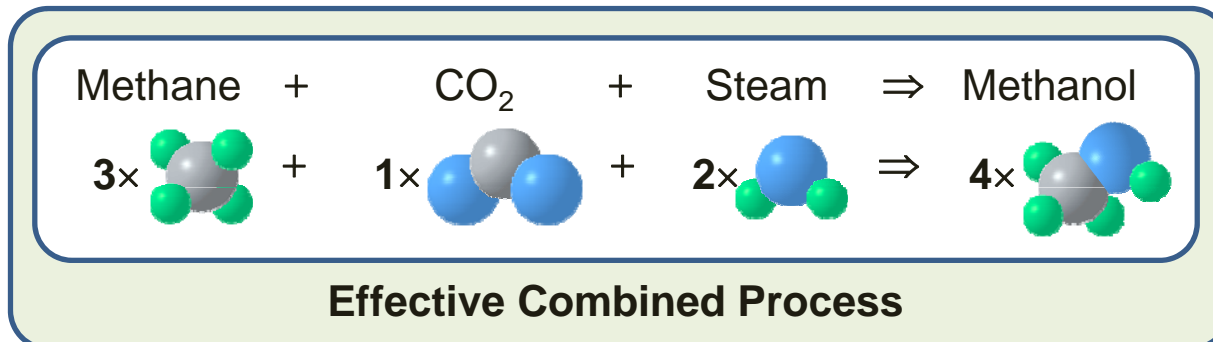
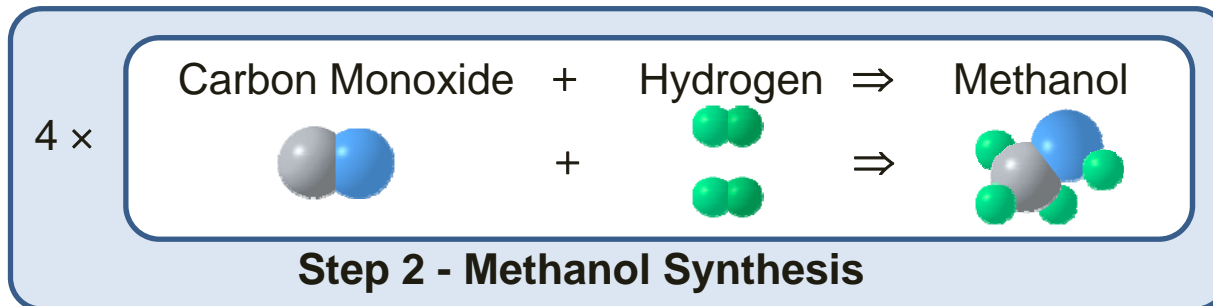
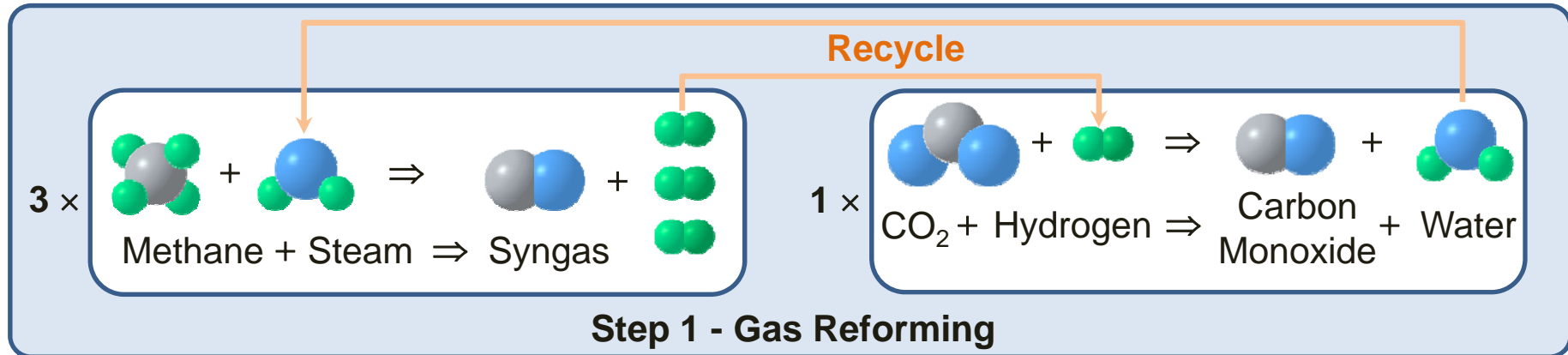


- FLNG motion impacts effectiveness of CO₂ removal processes *
- CO₂ disposal is an issue in light of climate change / CPRS
- Tassie Shoal Project solves both problems




* A.M. Tan, BASF 16 July 2008

Chemical sequestration of CO₂

Alchemy



Legend

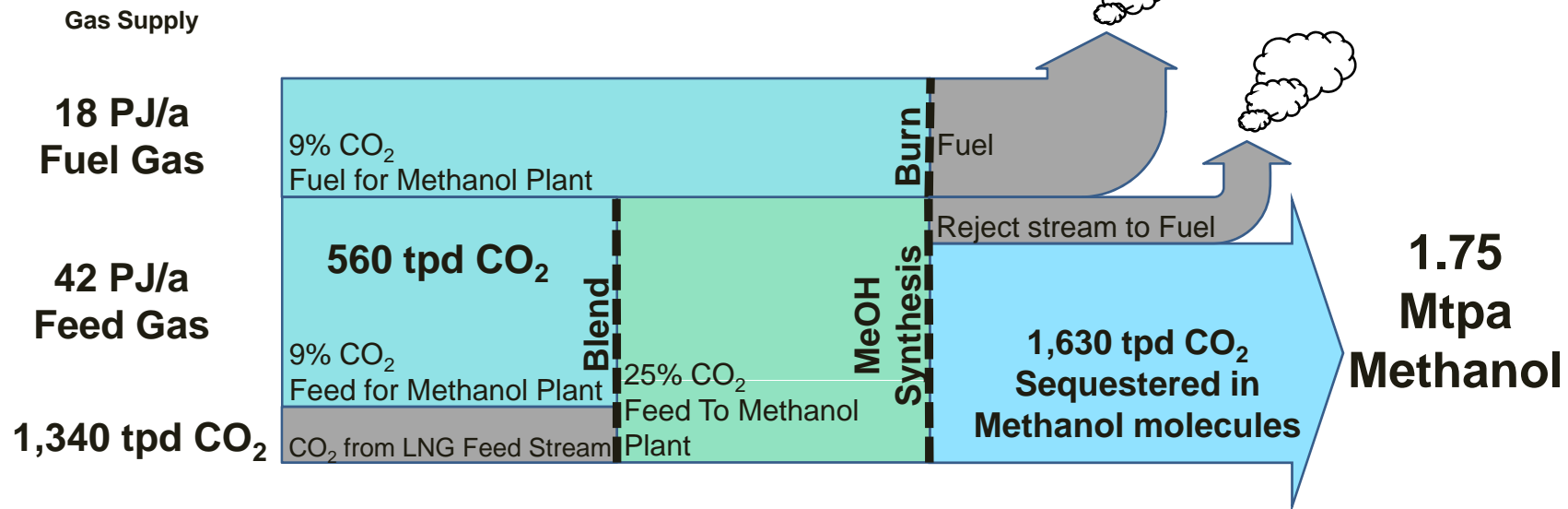
-  = Hydrogen
-  = Carbon
-  = Oxygen

CO₂ sequestration into methanol

Achieves lower CO₂ intensity than geo-sequestration

tpd CO ₂	Source
249	(carried)
2,703	(combustion)
2,952	(total)

tpd CO ₂	Source
270	(carried)
816	(combustion)
1,086	(total)



- Gorgon LNG based on 9% CO₂ gas with geo-sequestration = **0.35 tCO₂/tLNG** *
- Single Methanol Plant = **0.33 tCO₂/tLNG**
- Chinese coal based methanol production is swing producer and emits >1.7 times CO₂ per tonne of methanol compared with MEO proposed process
- Up to 80% of methanol ends up in chemically inert products (resins, MDF, glues, plastics etc)

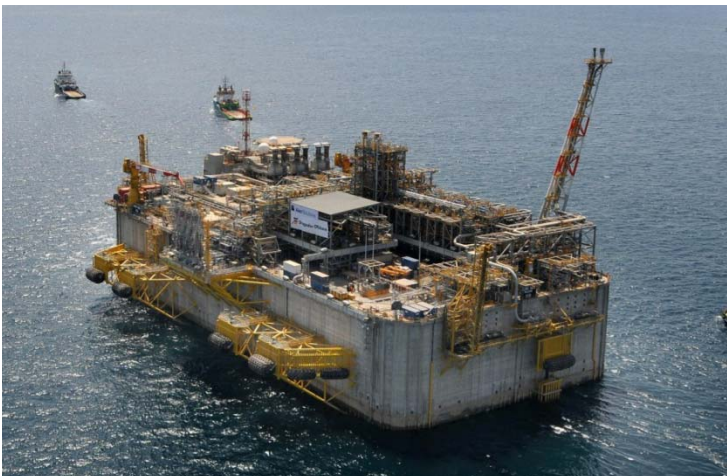
* (Source: Gorgon EIS)

Methanol plant on concrete GBS

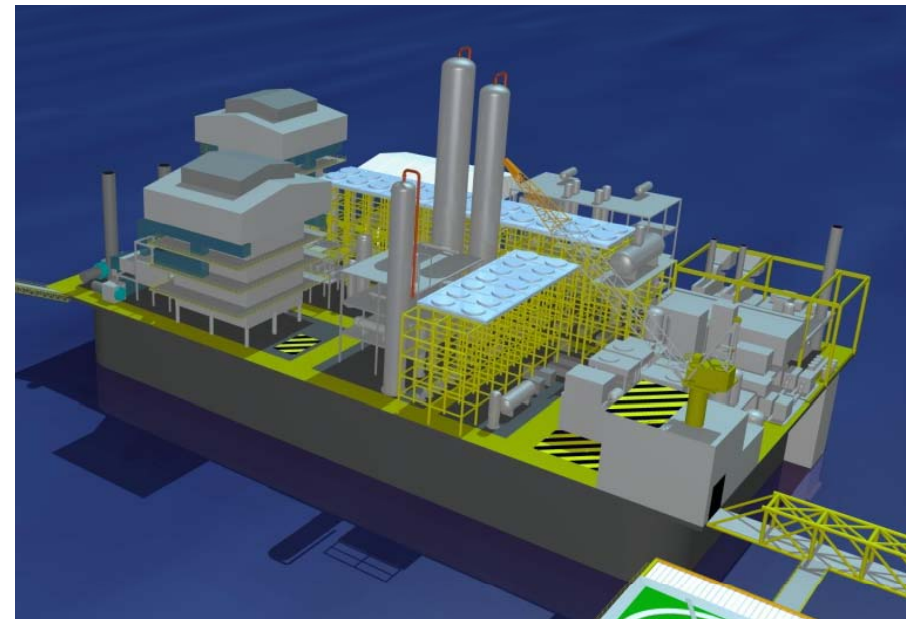
Combination of two proven technologies



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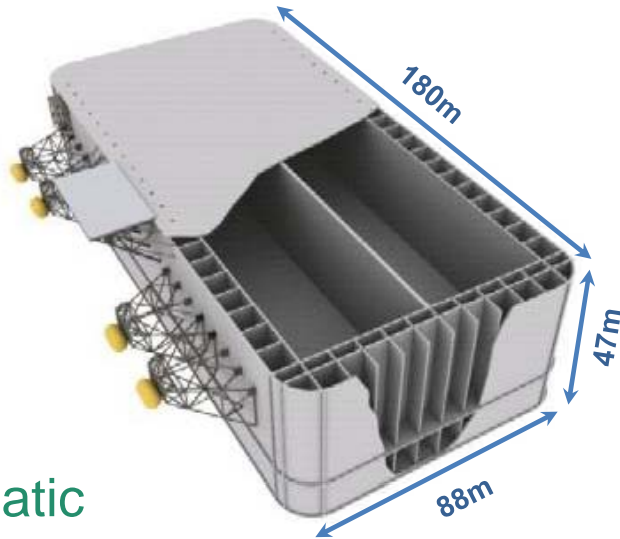
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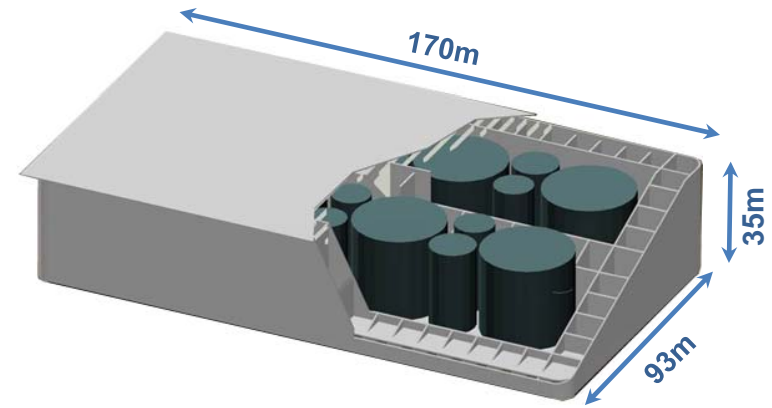
- Plant based on Davy Process Technology M5000 plant operating in Trinidad
- GBS builds on the lessons of ExxonMobil's Adriatic Re-gas terminal

Concrete GBS with internal storage

ExxonMobil Adriatic re-gas terminal



Adriatic



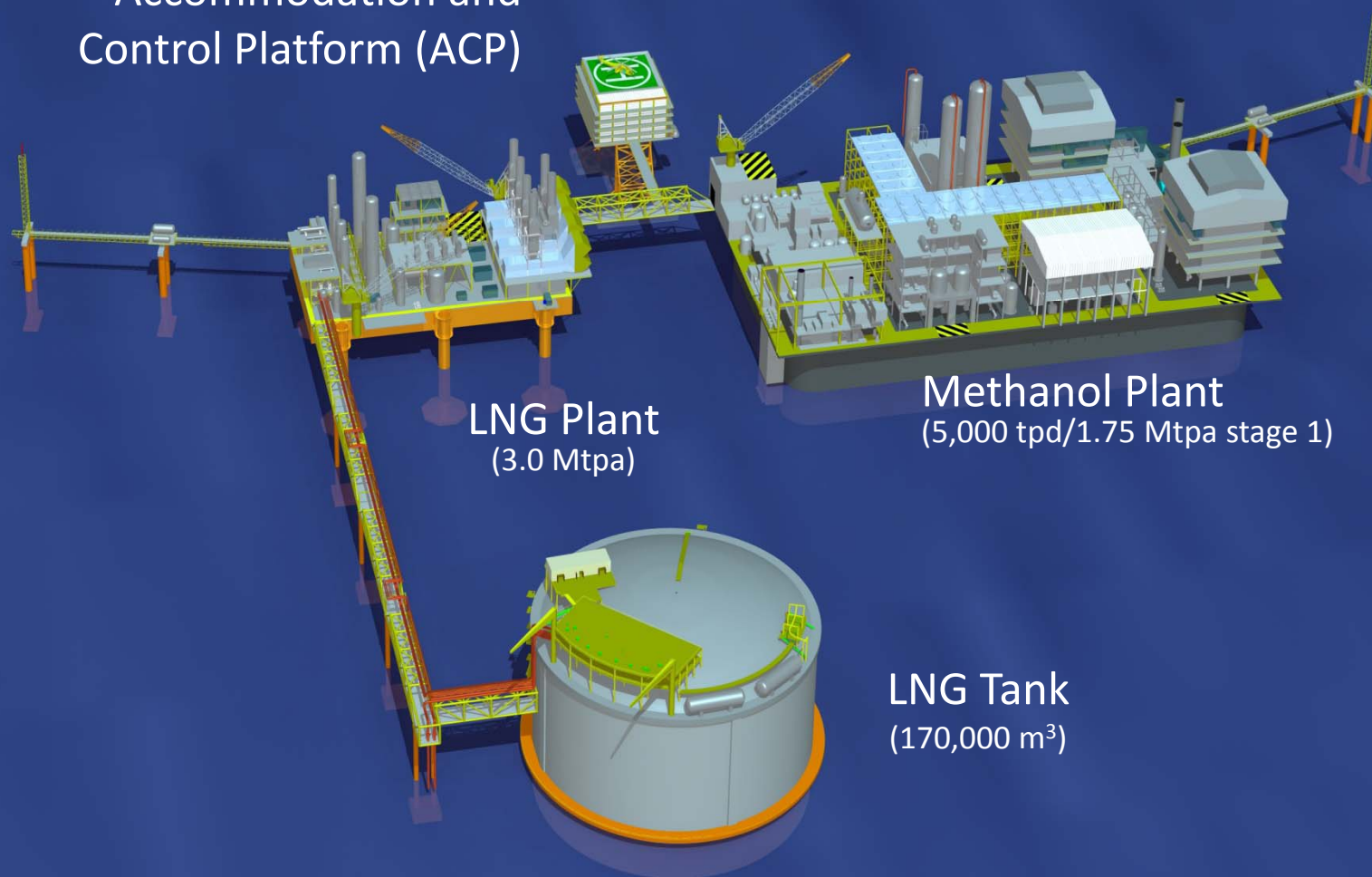
Tassie Shoal Methanol Plant GBS



Timor Sea Projects

At Tassie Shoal

Accommodation and
Control Platform (ACP)



LNG Plant
(3.0 Mtpa)

Methanol Plant
(5,000 tpd/1.75 Mtpa stage 1)

LNG Tank
(170,000 m³)



The Tassie Shoal Project

Stepping stones to FLNG

Recap:

- Uses liquefaction technology originally developed for FLNG
- Will prove FLNG technology in offshore environment
- Movement issues avoided
- Substantial cost savings
- Environmental approvals in place
- Complementary CO₂ sequestration plant generates additional revenue
- Storage, ACP and load-out can be shared with future developments
- Provides the nucleus for regional development

Won't work everywhere – but it will work on Tassie Shoal